## Isolation of accelerator produced <sup>140</sup>Nd from macro-amount of Ce and Pr by means of cation-exchanger chromatography

K.P. Zhernosekov<sup>1</sup>, D.V. Filosofov<sup>2</sup>, N.A. Lebedev<sup>2</sup>, S.M. Qaim<sup>3</sup>, F. Rösch<sup>1</sup>

<sup>1</sup>Institut für Kernchemie, Johannes Gutenberg-Universität, D-55128 Mainz, Germany; <sup>2</sup>Joint Institute of Nuclear Research, LNP, 141980 Dubna; <sup>3</sup>Institute für Nuklearchemie, Forschungszentrum Jülich GmbH, Germany

Introduction: <sup>140</sup>Nd (100 % EC,  $T\frac{1}{2} = 3.37$  d) generates the short-lived intermediate  ${}^{140}Pr$  (49%  $\beta^+$ ,  $E_{max} = 2.4$ MeV,  $T\frac{1}{2} = 3.39$  m), which decays to stable <sup>140</sup>Ce. This system was supposed to be useful as generator or in vivo generator systems for PET [1]. A detailed study of  $^{141}$ Pr(p,2n) $^{140}$ Nd  $^{nat}Ce(^{3}He,xn)^{140}Nd$  and nuclear reactions was published recently [2]. The overall yields of <sup>140</sup>Nd are 12 and 210 [MBq/µA·h], respectively. Whereas irradiation of praseodymium provide higher overall yields, chemical isolation of <sup>140</sup>Nd(III) seems to be more efficient if cerium is irradiated. In this work both routes were applied for the production and separation of <sup>140</sup>Nd. Radiochemical separations were performed by means of cation-exchange chromatography according to Nd(III)/Ce(III) and Nd(III)/Pr(III) separations.

Experimental: <sup>140</sup>Nd was produced irradiating natural cerium oxide with 36 MeV <sup>3</sup>He-particles and irradiating praseodymium oxide with protons of 30 MeVat the CV28 cyclotron of the Forschungszentrum Jülich. Irradiated CeO<sub>2</sub> (500 mg  $\equiv$  2.9 mmol) was dissolved in HCl<sub>conc</sub> solutions by reduction of Ce(IV) to Ce(III) in the presence of I ions. The target material was boiled in ~ 40 ml of HCl<sub>conc</sub> with addition of 0.5-1 g KI within 1-1.5 hours. After complete dissolution, the remaining bulk (~ 10 ml) was adjusted up to 110 ml with H<sub>2</sub>O and filtrated on a standard glass filter. The solution was loaded on a chromatography column of 400×20 mm dimension (V<sub>fr</sub> ~ 127 ml), filled with Bio-Rad AG 50W-X8, 200-400 mesh in hydrogen form. The resin was washed with about 600 ml of 0.5 M NH<sub>4</sub>Cl to transfer the cationexchanger into the NH<sub>4</sub><sup>+</sup>-form. Chromatographic separation was performed by isocratic elution (Fig. 1).  $^{140}$ Nd(III) was selectively eluted with 0.30 M  $\alpha$ -HIB solution. Ce(III) was washed down at the concentration 0.40 M. The eluate was fractionated by 30 ml. Irradiated  $Pr_2O_3$  (200 mg = 0.6 mmol) was dissolved in 5 ml of  $HCl_{conc}$  by heating within 20 – 30 minutes. After addition of  $^{142/141}$ PrCl<sub>3</sub> and 5 mmol of NH<sub>4</sub>Cl the mixture was evaporated under argon atmosphere. The dried residue was dissolved in 20 ml of H<sub>2</sub>O to achieve a pH 1 - 2 and filtrated on a standard glass filter. The primary chromatography column had optimised dimension of 390×16.1 mm (V<sub>fr</sub> ~ 80 ml), filled with Bio-Rad AG 50W-X8, 200-400 mesh. To improve separation conditions, isotopes were loaded onto the cationexchanger directly in NH<sub>4</sub><sup>+</sup> form. The resin was washed with 120 ml of 0.20 M  $\alpha\text{-HIB}$  solution.  $^{140}Nd(\text{III})$  was selectively eluted with 0.29 M  $\alpha$ -HIB solution. Pr(III) was washed down at the concentration 0.40 M (Fig. 2). The eluate was fractionated by 12 ml. In both cases final purification of <sup>140</sup>Nd(III) could be performed on a small Aminex A6 column (100×2 mm), using  $\alpha$ -HIB eluent systems.



Figure 1. <sup>140</sup>Nd(III)/Ce(III) separation. Profiles of an isocratic elution on the primary chromatography column.



Figure 2. <sup>140</sup>Nd(III)/Pr(III) separation. Profiles of elution on the primary chromatography column

**Results**: The isolation of <sup>140</sup>Nd(III) by means of cationexchanger chromatography from the target materials was evidently more efficient if cerium oxide is irradiated (*decontamination factor*  $\geq 10^8$ ). However, superior purification within two steps only could be performed for the <sup>140</sup>Nd(III)/Pr(III) system (*decontamination factor*  $\geq$  $7 \cdot 10^5$ ). In both cases the evaluated amounts of the target material remaining was below 1 nmol. With consideration of higher <sup>140</sup>Nd overall yield, the <sup>141</sup>Pr(p,2n)<sup>140</sup>Nd production route seems to be absolutely superior.

## References

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